

Power Vision Engineering



Risk of Low Pressure at Penstock Top of Pumped Storage Power Plant in Pumping Mode

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Introduction

• Risk of low pressure at top penstock in PSPP:

Emergency shutdown (ESD) in pumping mode:









Introduction

• Risk of low pressure at top penstock in PSPP:

Pump-turbine detailed transient:







Introduction

• Risk of low pressure at top penstock in PSPP:

Pressure envelop along the penstock:



Case Study

• Risk of low pressure at top penstock in PSPP:

- Low pressure risk emphasized by:
 - High surge tank inertia $L_h = \frac{l}{gA}$
 - High singular head losses at junction
 - High elevation point:
 - Sub-horizontal penstock after surge tank
 - gate valve
 - air valves

Air Valves Opening

• Pump Emergency Shutdown (ESD):

✓ Air valve modeling:

$$m = mo + \int_{0}^{t} \left(\frac{dm}{dt}\right) dt$$
 $V = \frac{mRT}{p}$ $pV^{n} = cste$

$$\int_{0}^{0} \left(\frac{dt}{dt} \right) \qquad p$$

$$(Wylie \& Streeter, 1993)$$

$$\left(\frac{dm}{dt} \Big|_{in} = C_{in} \cdot A_{in} \sqrt{7 p_o \rho_o} \left[\left(\frac{p}{p_o} \right)^{1.4286} - \left(\frac{p}{p_o} \right)^{1.714} \right] \qquad p_o > p > 0.53 p_o$$

$$\frac{dm}{dt} \Big|_{in} = C_{in} \cdot A_{in} \frac{0.686}{\sqrt{RT_o}} p_o \qquad p < 0.53 p_o$$

$$\frac{dm}{dt} \Big|_{out} = -C_{out} \cdot A_{out} \sqrt{\frac{7}{RT}} \left[\left(\frac{p_o}{p} \right)^{1.4286} - \left(\frac{p_o}{p} \right)^{1.714} \right] \qquad \frac{p_o}{0.53} > p > p_o$$

$$\frac{dm}{dt} \Big|_{out} = -C_{out} \cdot A_{out} \frac{0.686}{\sqrt{RT}} p \qquad p > \frac{p_o}{0.53}$$

 p_o, ρ_o, T_o : gas conditions outside R=287.6: gas constant [J/(kg·K°)]

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Air Valves Opening

• Pump Emergency Shutdown (ESD):

✓ Air valve modeling:

Conclusions and Recommendations

- Top penstock are subjected to low pressure in case of pump emergency shutdown
- Prediction requires detailed simulation model with realistic pump-turbine characteristic
- Surge tank may feature:
 - ✓ Inertia of the water column $L_h = \frac{l}{gA}$
 - Junction head losses
- Air valves opening at penstock top:
 - Prevent from negative pressure and cavitation if well sized (risk of penstock collapse or water column separation)
 - ✓ Also induce risk of over pressure!!! => penstock burst
- Address carefully the top penstock pressure (min and max) with appropriate modeling including sufficient safety and error margin!

Thank you for your attention!

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